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## **Question Paper Code: X60843**

B.E./B.Tech. DEGREE EXAMINATIONS, NOVEMBER/DECEMBER 2020

Fourth/Fifth/Sixth Semester

Mechanical Engineering

ME 2251/ME 1251/10122 ME 502/ME41/080120015 – HEAT AND MASS TRANSFER (Common to Mechanical and Automation Engineering)

(Regulations 2008/2010)

(Also Common to PTME 2251 – Heat and Mass Transfer for B.E. (Part-Time) Sixth semester – Mechanical Engineering – Regulations 2009)

Time: Three Hours Maximum: 100 Marks

Use of Heat and Mass Transfer Tables permitted Answer ALL questions

PART - A

 $(10\times2=20 \text{ Marks})$ 

**(6)** 

- 1. State Fourier's Law of conduction.
- 2. What is meant by lumped heat capacity analysis?
- 3. Air at 27°C and 1 atmospheric flows over a flat plate at a speed of 2 m/s. Calculate boundary layer thickness at distance 40 cm from loading edge of plate. At 27°C viscosity (air) =  $1.85 \times 10^{-5}$  kg m/s.
- 4. A square plate 40 cm × 40 cm maintained at 400 K is suspended vertically in atmospheric air at 300 K. Determine the boundary layer thickness at trailing edge of the plate.
- 5. How does laminar flow differ from turbulent flow?
- 6. What is burnout point in boiling heat transfer? Why is it called so?
- 7. Define LMTD of a heat exchanger.
- 8. What is thermal radiation? What is its wavelength band?
- 9. State Fick's Law of diffusion.
- 10. Write down the analogous terms in heat and mass transfer.

PART – B (5×16=80 Marks)

- 11. a) i) Derive general heat conduction equation in Cartesian coordinates. (10)
  - ii) Compute the heat loss per square meter surface area of a 40 cm thick furnace wall having surface temperatures of 300°C and 50°C if the thermal conductivity k of the wall material is given by  $k = 0.005 \text{ T} 5 \times 10^{-6} \text{ T}^2$  where T = temperature in °C.

(OR)

- b) i) A furnace wall consists of 200 mm layer of refractory bricks, 6 mm layer of steel plate and a 100 mm layer of insulation bricks. The maximum temperature of the wall is 1150°C on the furnace side and the minimum temperature is 40°C on the outermost side of the wall. An accurate energy balance over the furnace shows that the heat loss from wall is 400 W/m². It is known that there is a thin layer of air between the layers of refractory bricks and steel plate. Thermal conductivities for the three layers are 1.52, 45 and 0.138 W/m°C respectively. Find
  - 1) To how many millimeters of insulation brick is the air layer equivalent?
  - 2) What is the temperature of the outer surface of the steel plate. (8)
  - ii) Find out the amount of heat transferred through an iron fin of length 50 mm, width 100 mm and thickness 5 mm. Assume k = 210 kJ/mh°C and h = 42 kJ/m²h°C for the material of the fin and the temperature at the base of the fin as 80°C. Also determine the temperature at tip of the fin, if atmosphere temperature is 20°C. (8)
- 12. a) i) Define velocity boundary layer and thermal boundary layer. (4)
  - ii) Air at 200 kPa and 200°C is heated as it flows through a tube with a diameter of 25 mm at a unit length of the tube. If a constant heat flux condition is maintained at the wall and the wall temperature is 20°C above the air temperature, all along the length of the tube. How much would the bulk temperature increases over 3 m length of the tube. (12)

(OR)

- b) i) A 0.5 m high flat plate of glass at 93°C is removed from an annealing furnace and hung vertically in the air at 28°C. 1 atm. Calculate the initial rate of heat transfer to the air. The plate is 1 m wide. (10)
  - ii) A fine wire having a diameter of 0.02 mm is maintained at a constant temperature of 54°C by an electric current. The wire is exposed to air at 1 atm and 0°C. Calculate the electric power necessary to maintain the wire temperature if the length is 50 cm. (6)
- 13. a) Discuss briefly the pool boiling regimes of water at atmospheric pressure. (OR)
  - b) i) What are the different types of fouling in heat exchangers? (4)
    - ii) Hot exhaust gases which enter a cross-flow heat exchanger at 300°C and leave at 100°C are used to heat water at a flow rate of 1 kg/s from 35 to 125°C. The specific heat of the gas is 1000 J/kg.K and the overall heat transfer coefficient based on the gas side surface is 100 W/m².K. Find the required gas side surface area using the NTU method and LMTD method. (12)
- 14. a) Consider a cylindrical furnace with outer radius = 1 m and height = 1 m. The top (surface1) and the base (surface 2) of the furnace have emissitives 0.8 and 0.4 and are maintained at uniform temperatures of 700 K and 500 K respectively. The side surface closely approximates a black body and is maintained at a temperature of 400 K. Find the net rate of radiation heat transfer at each surface during steady state operation.



- b) Emissivities of two large parallel plates maintained at 800°C and 300°C are 0.3 and 0.5 respectively. Find the net radiant heat exchange per square meter for these plate. Find the percentage reduction in heat transfer when a polished aluminium radiation shield ( $\epsilon$  = 0.05) is placed between them. Also find the temperature of shield.
- 15. a) Explain different modes of mass transfer and derive the general mass diffusion equation in stationary media.

(OR)

b) Explain Reynold's number, Sherwood number, Schmidt number and solve the following:

A vessel contains a binary mixture of oxygen and nitrogen with partial pressures in the ratio 0.21 and 0.79 at 15°C. The total pressure of the mixture is 1.1 bar. Calculate the following:

i) Molar concentrations	(4)
ii) Mass densities	(4)
iii) Mass Fractions	(4)
iv) Molar fractions of each species.	(4)